

ultrastable zeolite Y (Si/Al = 5 to 50 ratio of Si to Al in zeolite Y) and Beta (Si/Al = 10 – 120 ratio of Si to Al in zeolite Beta), and

separating the products formed in vapour phase.

2. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein said substrate and alkylating agent are contacted with said solid acid zeolite catalyst at a temperature in the range of 80 - 250°C and for a period of at least 1 hour.

3. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein the product is separated from the vapour phase by condensation at a temperature in the range of 0 - 3°C.

4. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein the substrate is selected from the group consisting of *o*-xylene, *m*-xylene, *p*-xylene and any mixture thereof.

5. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein the Si/Al ratio in said catalyst is between 5 to 20.

6. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein the alkylating agent is selected from the group consisting of propylene and propyl alcohols ~~such as isopropanol and n-propanol~~.

7. (Currently Amended) A process as ~~claimed~~ in claim 2 wherein the temperature of the reaction is in the range of 100 - 200°C.

8. (Currently Amended) A process as ~~claimed~~ in claim 2 wherein the temperature of the reaction is in the range of 120 - 180°C.

9. (Currently Amended) A process as ~~claimed~~ in claim 1, wherein the molar ratio of xylene substrate to the alkylating agent in the feed is in the range of from 1:2 to 20:1.
10. (Currently Amended) A process as ~~claimed~~ in claim 9 wherein the molar ratio of xylene substrate to the alkylating agent is in the range of 1:1 to 10:1.
11. (Currently Amended) A process as ~~claimed~~ in claim 9 wherein the molar ratio of xylene substrate to the alkylating agent is in the range of 1:2 to 5:1.
12. A process as ~~claimed~~ in claim 1 wherein the weight hourly space velocity (WHSV) of the feed is in the range of 0.5 to 30 h⁻¹.
13. (Currently Amended) A process as ~~claimed~~ in claim 12 wherein the weight hourly space velocity (WHSV) of the feed is in the range of 1 to 20h⁻¹.
14. (Currently Amended) A process as ~~claimed~~ in claim 12 wherein the weight hourly space velocity (WHSV) of the feed is in the range of 2 to 10h⁻¹.
15. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein the alkylation reaction is carried out in a fixed bed reactor or a batch reactor.
16. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein *p*-xylene is alkylated using isopropanol in the presence of zeolite beta catalyst.
17. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein *m*-xylene and *o*-xylene are alkylated using isopropanol as the alkylating agent in the presence of ultrastable zeolite Y (USY) as catalyst.

18. (Currently Amended) A process as ~~claimed~~ in claim 1 wherein a mixture of *p*-xylene and isopropyl alcohol in a molar ratio of 4:1 is reacted in a fixed bed reactor in the presence of ultrastable zeolite Y catalyst.